

French HLW vitrification history and major achievements

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Regis DIDIERLAURENT
Sumglass 2023



Summary

1. French vitrification history
2. La Hague vitrification lines achievements
3. Latest development

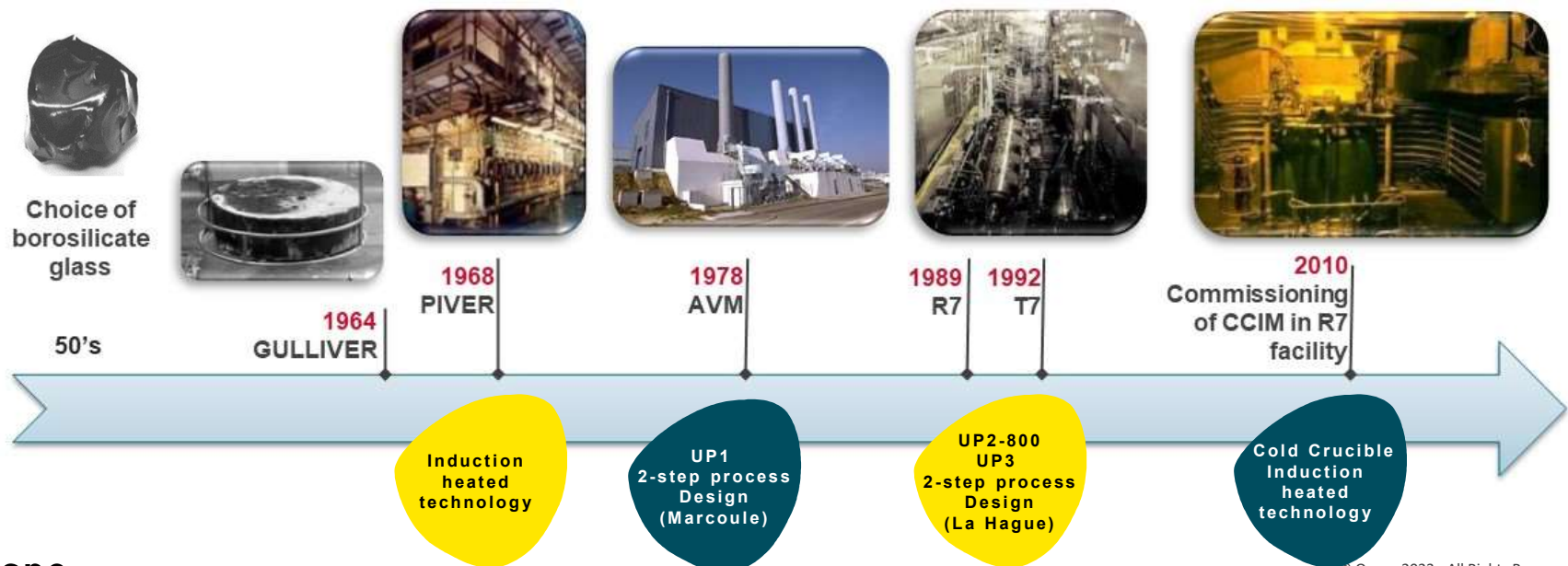
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French vitrification history

Major French Vitrification Technology Milestones

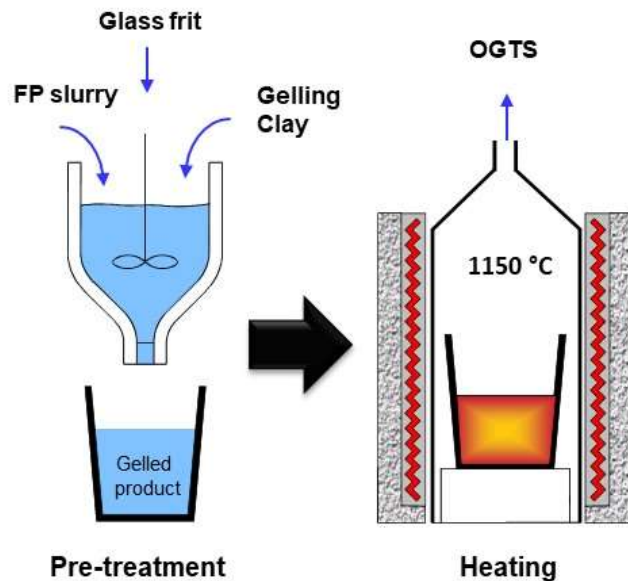
Vitrification of High-Level Waste (HLW) is the internationally recognized standard to:

- Minimize the final waste volume
- Minimize the impact to the environment resulting from waste disposal



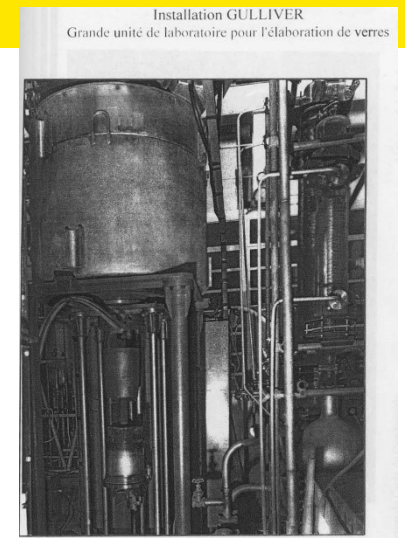
Historical overview GULLIVER Process (1964 – 1967)

1st Large Scale Active Pilot



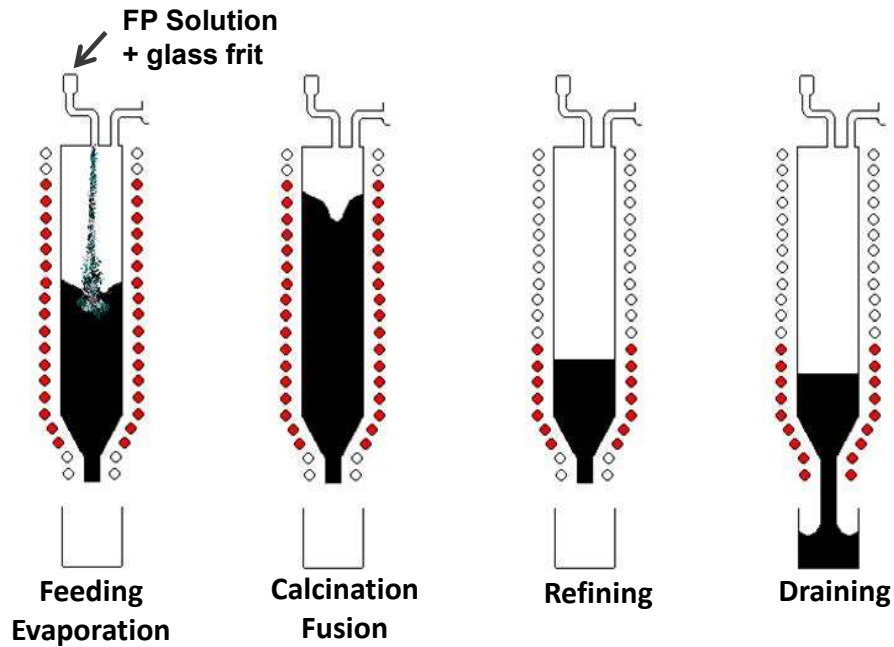
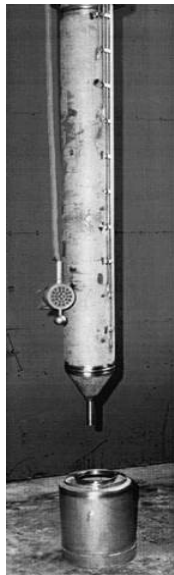
► Batch process in graphite crucible

- Resistance heating
- Controlled cooling
- Production: ~50 blocks of 4 kg
- 2 000 to 3 000 Ci/L of glass



Historical Overview PIVER Process (1968 – 1980)

1st Industrial Unit



► Batch process in graphite crucible

- Induction heating
- Draining by the bottom
- Throughput: 5 kg/h
- Production: 12 metric tons of glass



Historical Overview

2-Step Process Reference Design

AVM – Operated by Orano from 1978 to 2009 (Marcoule)

1 vitrification line

- ~ 3 300 canisters produced
- ~ 1 220 metric tons of glass produced
- ~ 22 10⁶ TBq vitrified

R7 / T7 – Operated by Orano since 1989 (La Hague plant)

2 vitrification facilities (6 lines)

IHMM (end of 2021)

- ~ 24 100 canisters produced
- ~ 9 600 metric tons of glass produced
- ~ 368 10⁶ TBq vitrified

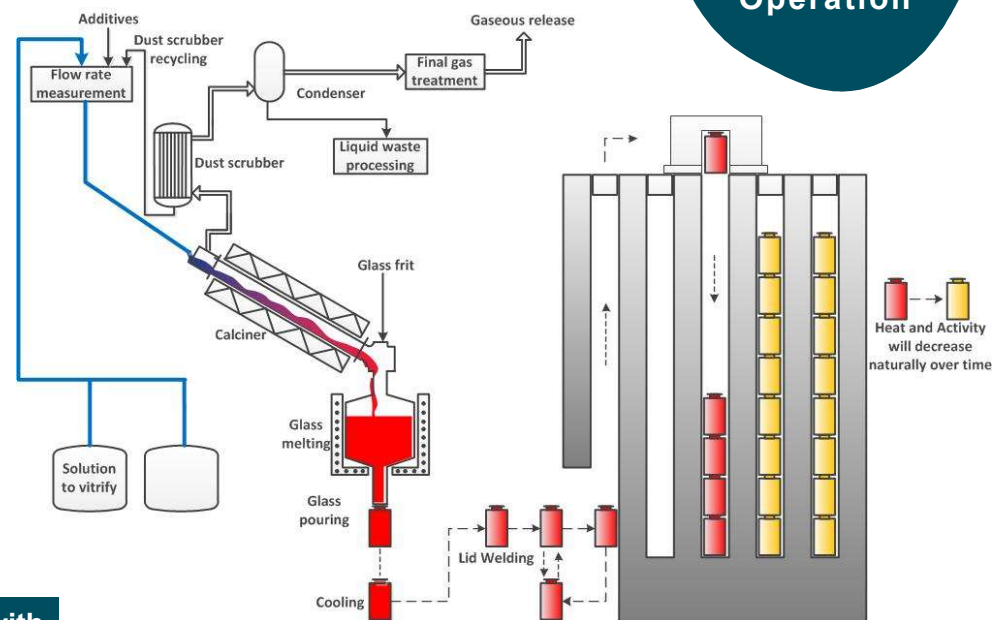
CCIM (end of 2021)

- ~ 1 000 canisters produced

Very High-Level Waste management with significant incorporation rate into the glass

→ Around 1 Ci/g

Over 40 years of Industrial Operation

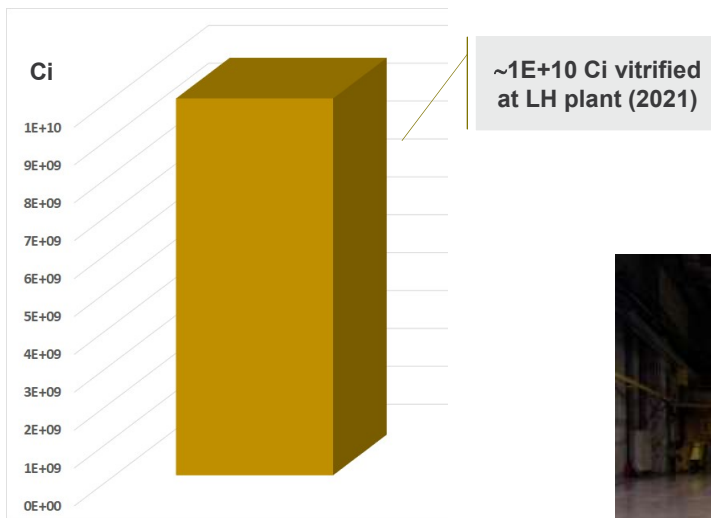


Process also implemented at WVP Sellafield



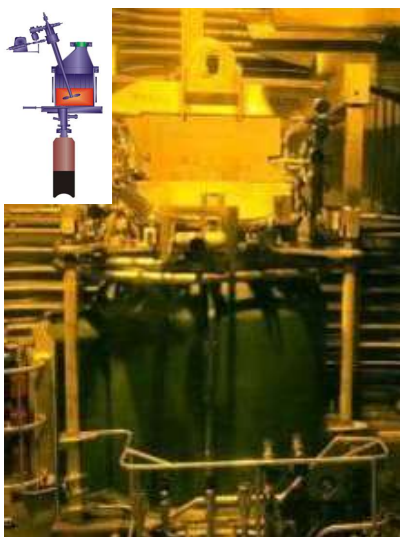
Orano La Hague Vitrification Track Records

Significant amount of radioactivity vitrified over the years



Main vitrification technologies developed

CCIM



**Cold Crucible
Direct induction**

In operation since 2010

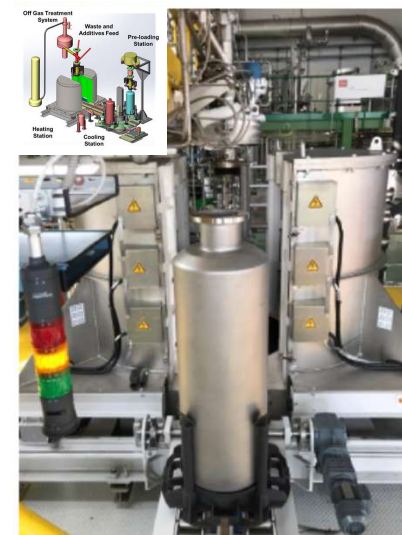
IHMM



**Metallic Melter
Indirect induction**

In operation since 1978

In-Can Melter



**Resistance heating
Thermal homogenization**

*Full scale pilot
commissioned in 2020*



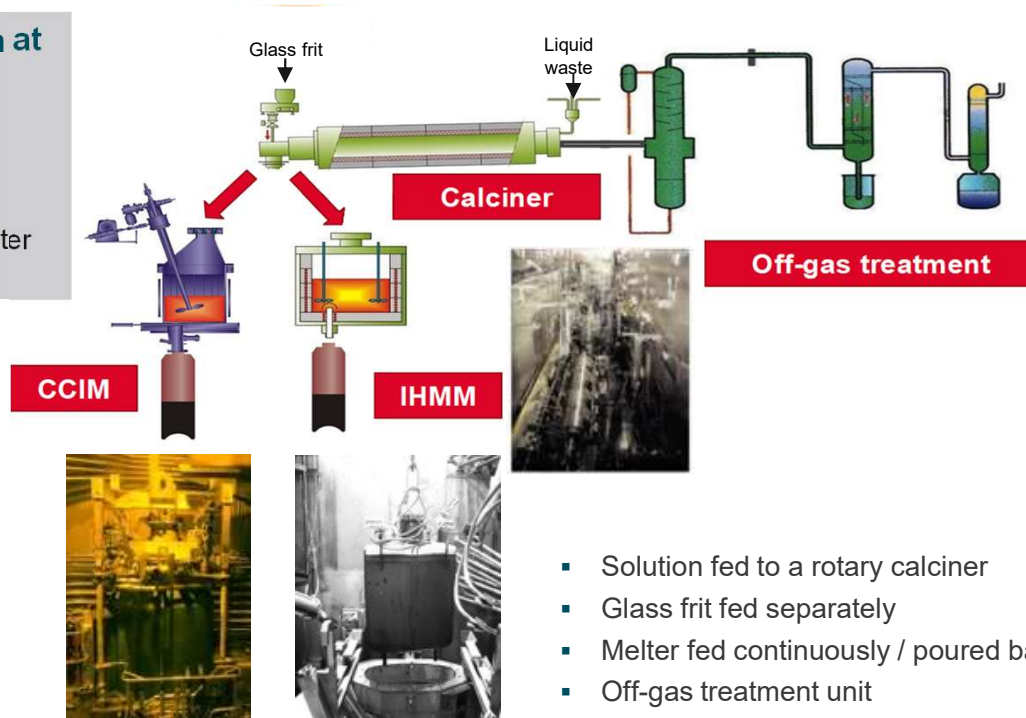
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La Hague vitrification lines achievements

R7/T7 Vitrification 2-Step Process

► **2 vitrification facilities in operation at La Hague plant**

- Up to 1 100 canisters/year
- 5 lines with **Induction Heated Metallic Melter** (6 lines from 1989 to 2008)
- 1 line with **Cold Crucible Induction Melter** (commissioned in 2010)



- Solution fed to a rotary calciner
- Glass frit fed separately
- Melter fed continuously / poured batchwise
- Off-gas treatment unit

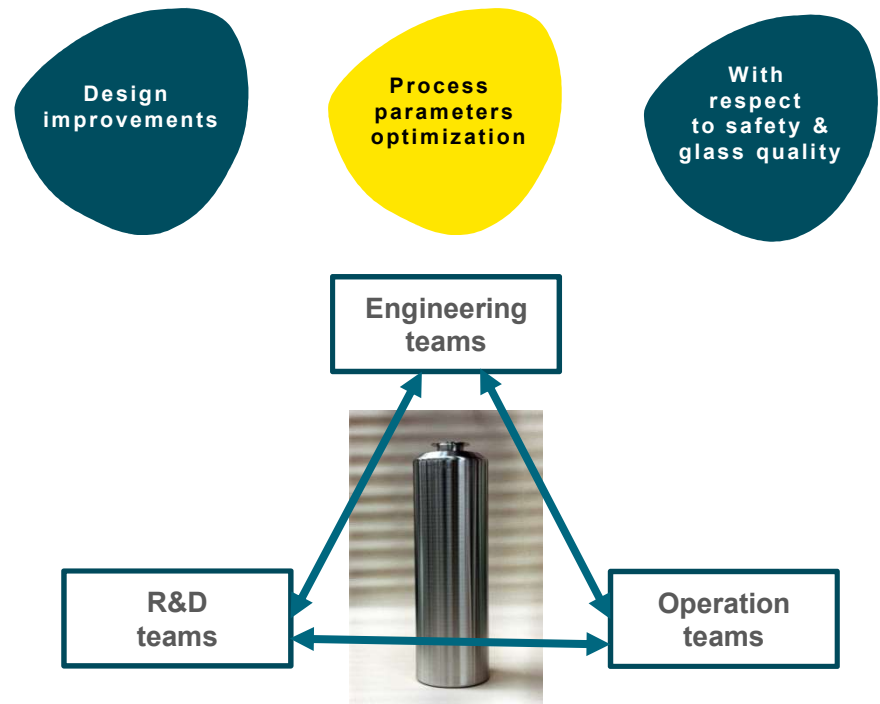


R7/T7 Continuous Improvement Policy

► Implementation of several improvement programs since R7 & T7 commissioning

► Major improvements/achievements:

- ↗ Calciner treatment capacity from 60 L/h to 105 L/h
- ↗ Calciner reliability and lifetime
- ↗ Noble Metals incorporation & glass throughput
- ↗ Melter (IHMM) lifetime by 400 %
- ↗ Overall reliability and remote in-cell maintainability
- Implementation of a CCIM in R7
- Adaptation of glass formulation for effluents to be vitrified



| | | | | | | |
|--|---|---|---|--|---|--|
| | | | | | | |
| 1986 300 AQ 016 • HA Glass specification for UOX FP • IHMM | 2007 300 AQ 60 • HA Glass specification for UOX FP • New alpha activity limit • IHMM | 2007 300 AQ 061 • IL Glass specification for Intermediate Level waste coming from D&D operations • CCIM | 2011 300 AQ 059 • HA Glass-ceramics specification for LMO FP • CCIM | 2012 300 AQ 063 • HA Glass specification for UOX FP • CCIM | 2017 DIRP SP 12 00082 • Pieces of HA Glass-ceramics specification for pieces of HA Glass-ceramics filled with sand | 2021 DIRP SP 15-00258 • HA Glass specification for UOX FP • New alpha activity limit • IHMM |
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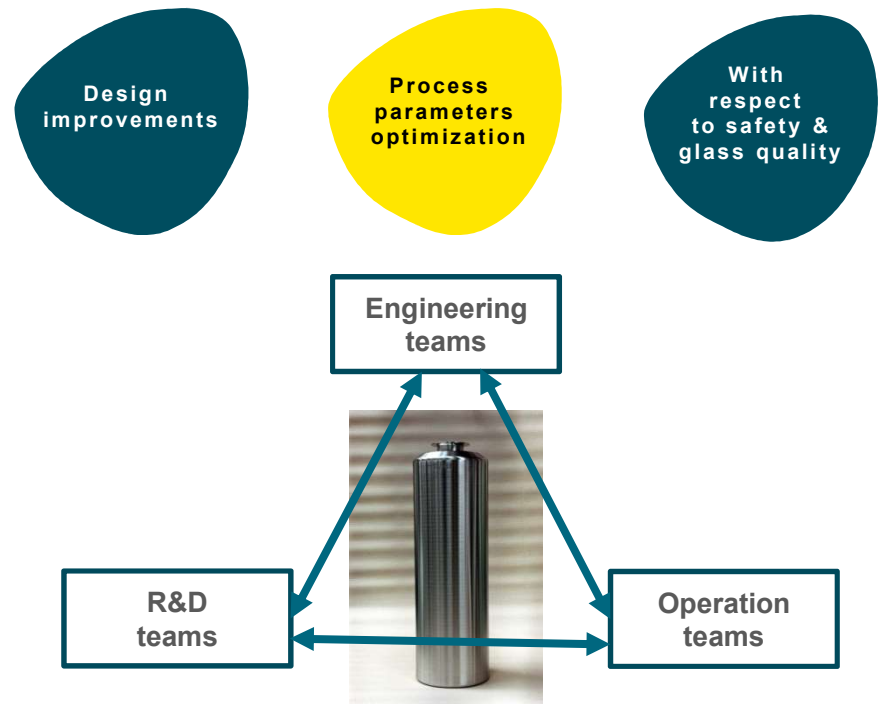


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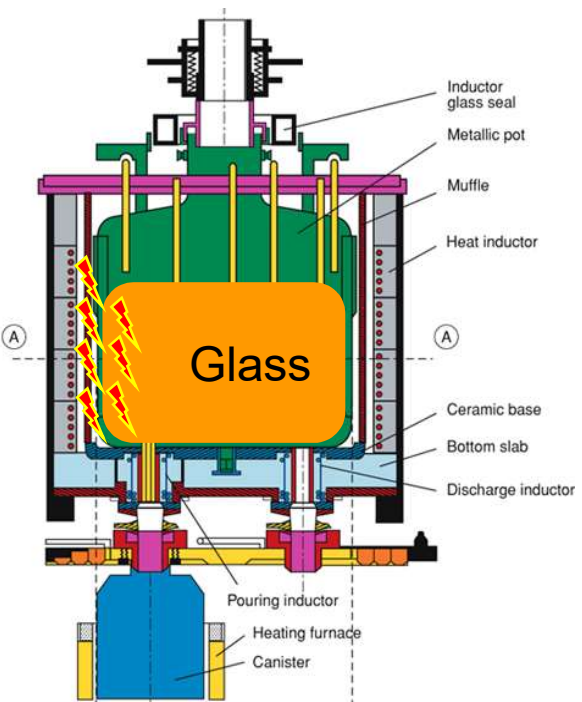
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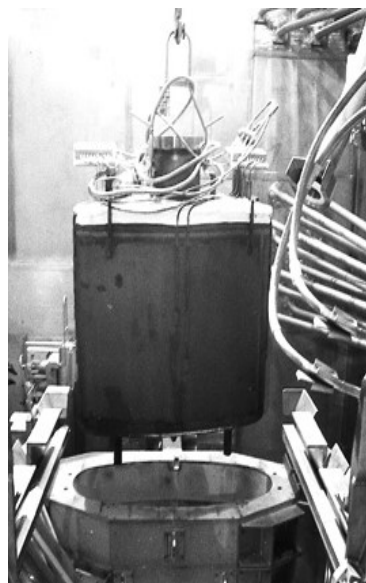
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| | | | | | | |



Induction Heated Metallic Melter (IHMM)



IHMM principles



IHMM in hot cell

Design Principles

- Inductive joule effect into metallic wall
- Thermal flux from metallic wall to molten glass
- Mixing ensured by bubbling and stirring

Process operation

- $T^\circ \sim 1100\text{ }^\circ\text{C}$
- Calcine fed
- Continuous feeding / Batchwise pouring

TRL 9

- Over 40 years of industrial operation
- Over 10 800 metric tons of glass produced

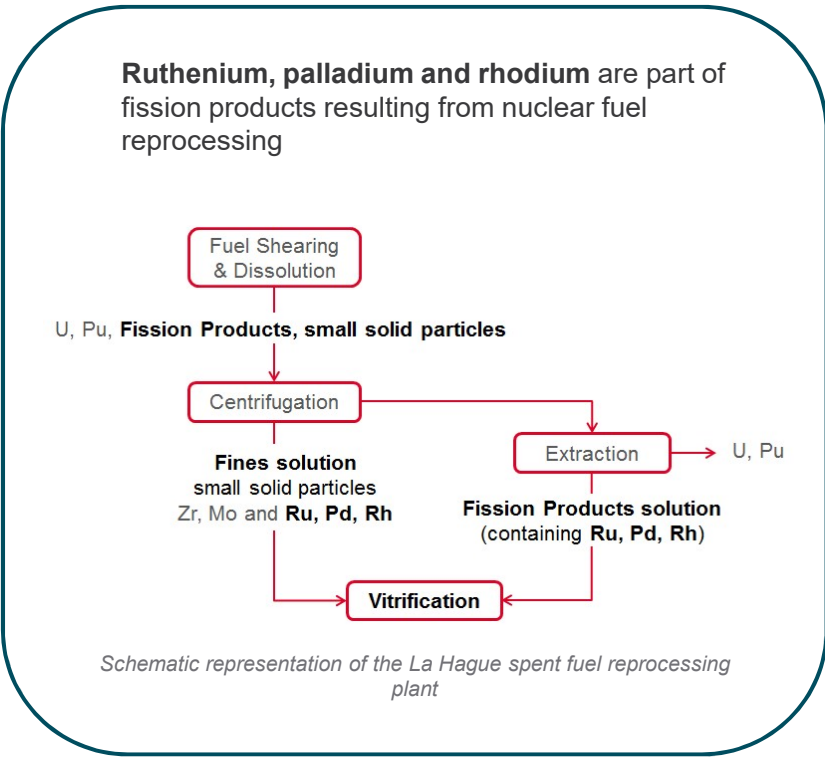
Wasteform

- Homogeneous borosilicate glass
- Around 1 Ci/g



Noble Metals Incorporation Challenges

Noble Metals Origin

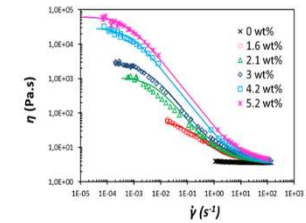


Noble Metals Challenges

- NM have Low solubility in the glass
- NM modify physical properties of the glass such as electrical and thermal conductivity and viscosity
- NM tend to settle to the bottom of the melter due to their high density
- NM can reduce the kinetics of the glass forming reaction

Potential issues

- Pouring problems
- Disruption of heating power distribution in the molten glass
- Risk of short-circuit (electrodes heating systems)
- Decrease of process throughput
- Increase of melter downtimes

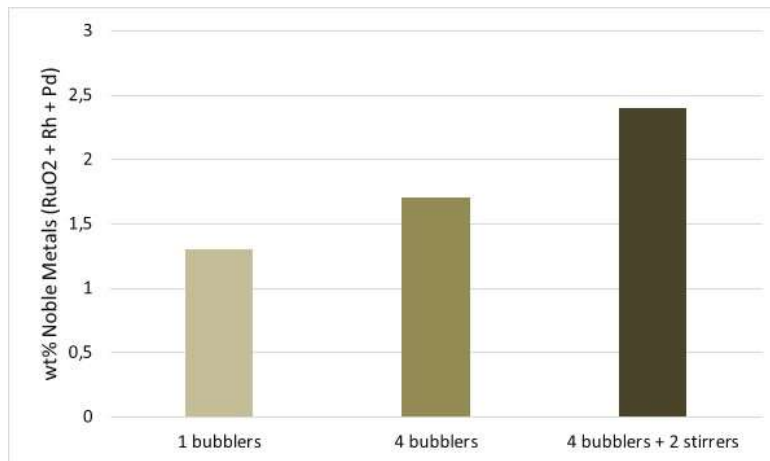


All high-level waste vitrification facilities have experienced operational problems arising from the presence of noble metals in the melter



IHMM Noble Metals Incorporation Improvement

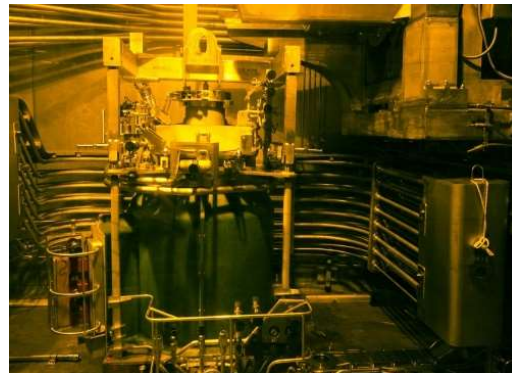
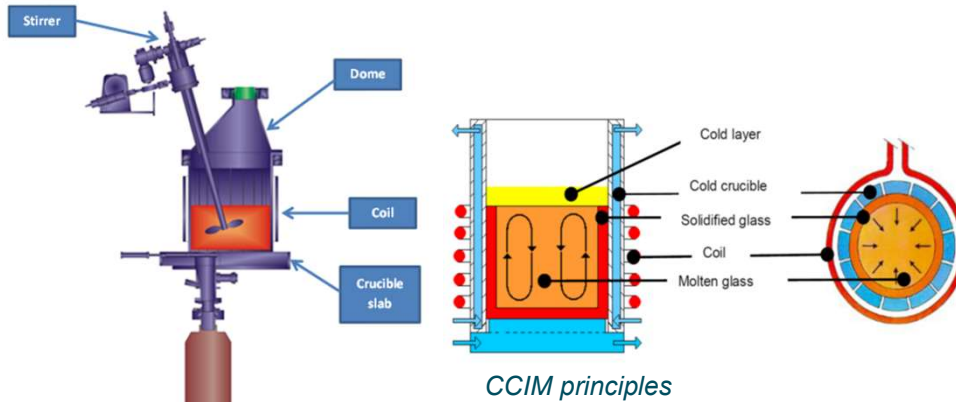
- ▶ **Several technological enhancements implemented to the melter design to improve mixing capability**
 - Initially → R7/T7 melters equipped with a single bubbler
 - 1990 → R7/T7 melters equipped with 4 bubblers
 - 1996 → R7/T7 melters equipped with 4 bubblers and mechanical stirring
- ▶ **2008-2014 → Optimization program to increase NM incorporation as well as glass throughput**
 - Analyze of industrial operation feedback
 - Identification of key process parameters affecting NM incorporation efficiency
 - Definition of new recommended operating parameters
 - Progressive implementation in the R7 & T7 facilities



- Enhancing thermal homogeneity
- Enhancing mixing of the glass melt (providing enough shearing to maintain the particles in suspension)
- Better spread of the glass frit and calcine fed to the melter
- Enhancing temperature management
- Improving operating modes



Cold Crucible Induction Melter (CCIM)



CCIM in hot cell

Design Principles

- Glass heated by Joule effect (Currents directly induced inside the molten glass)
- Cooled structures → Solidified layer of glass protecting the melter from the corrosive melt
- Mixing ensured by bubbling and stirring

Process operation

- T°: beyond 1300°C
- Solid or liquid fed
- Continuous feeding / Batchwise pouring
- High glass throughput reachable (higher T°)

TRL 9

- Over 12 years of industrial operation

Wasteform

- Homogeneous borosilicate glass
- Glass-ceramic
- High waste loading reachable (higher T°)



CCIM deployment in R7 facility

- ▶ 2010 → CCIM Commissioning in R7 facility - Line B
 - Vitrification of effluents from D&D operations
 - Requiring high T° to reach significant WL
 - Vitrification of legacy FP from reprocessing of U-Mo-Sn-Al spent fuel
 - High content of Mo & P making the glass extremely corrosive
 - Requiring high T° to reach significant WL



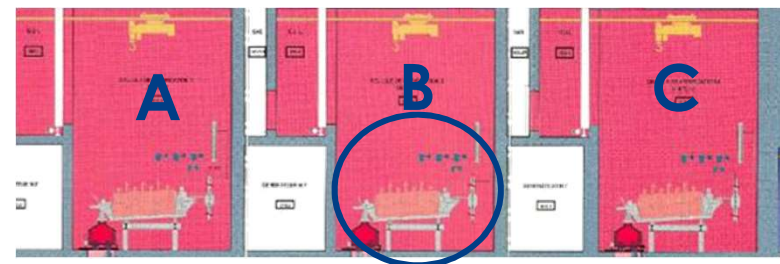
D&D glass



UMo glass-ceramic

Implemented in a very harsh environment with respect to challenging constraints

- Installed in place of an IHMM without impacting the existing structures and upstream or downstream equipment
- Installed in a highly radioactive cell into which human access was prohibited (whole work carried out remotely)
- Installed while lines A and C were in operation



CCIM Operation feedback

► Production

- Vitrification of effluents from the La Hague UP2-400 facility D&D operations → ~220 canisters
- Vitrification of the whole inventory of the UMo legacy FP → ~750 canisters
- Throughput achieved: ~ 135 kg/h/m²

► Improvements implemented since commissioning

- ↗ bubblers lifetime
- T° probes reliability enhancement (patent US8182146)
- Mechanical stirrer optimization

► Current status

- Vitrification of the very high-level fission products coming from the ongoing reprocessing activities at La Hague Plant
- Average incorporation rate of 1 Ci/g of glass
- Glass loaded with up to 3 wt% of NM (RuO₂ + Rh + Pd).

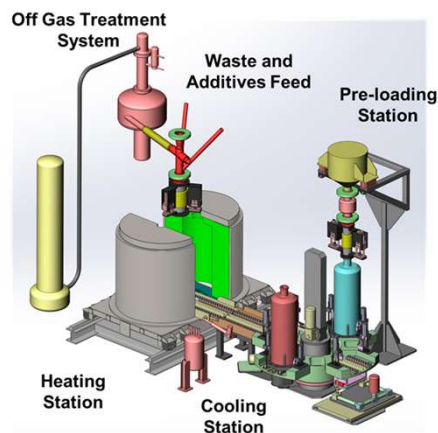
This achievement is the outcome of the continuous improvement policy implemented through a close collaboration between R&D, engineering teams and the industrial operator



3

Latest development

DEM&MELT In-Can Melter



DEM&MELT principles



DEM&MELT full-scale pilot

Design Principles

- ↻ Electrical resistance heating
- ↻ Canister used as the melter (no pouring device)
- ↻ Mixing ensured by heat convection
- ↻ Scalable

Process operation

- ↻ Operating temperature range ~ 100°C - 1150°C
- ↻ Solid or liquid fed
- ↻ Batch process

TRL 7

- ↻ Full scale pilot commissioned in 2020
- ↻ Design benefiting from proven technologies

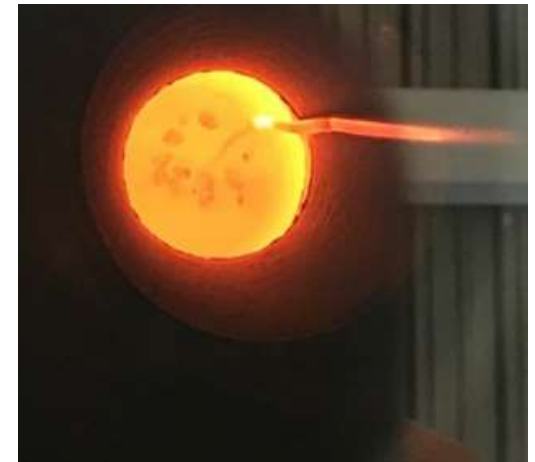
Wasteform

- ↻ Homogeneous borosilicate glass
- ↻ Composite matrices
- ↻ Waste encapsulation
- ↻ High waste loading reachable (up to 80 wt%)

State of Development

DEM&MELT full scale pilot commissioned in November 2020

- ▶ Proper operation on the whole perimeter: mechanical system, feeding system, melter, off-gas treatment system



Molten materials surface as observed during the DEM&MELT start-up test

State of Development

DEM&MELT full scale pilot commissioned in November 2020

- ▶ Proper operation on the whole perimeter: mechanical system, feeding system, melter, off-gas treatment system



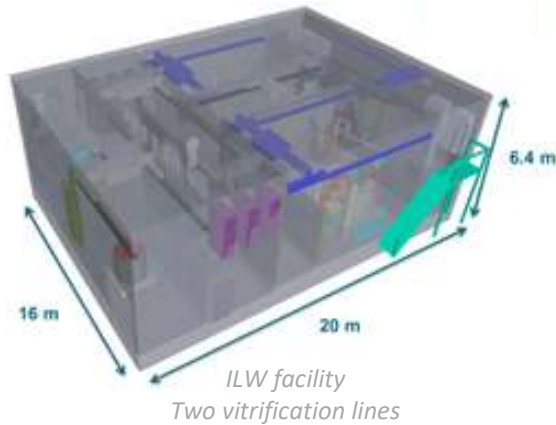
Mature and proven technologies from up stream functions to down stream functions with over 40 years of HA operation at Orano La Hague and CEA Marcoule

- ▶ **Remotely-controlled operation and maintenance functions**
TRL 9 – used in R7/T7 and ACC
- ▶ **Canister management functions**
TRL 9 – used in R7/T7 and ACC
- ▶ **Off-gas treatment system**
TRL 9 – used in R7/T7
- ▶ **Feeding systems**
TRL 9 – used in R7/T7
- ▶ **Auxiliary functions**
TRL 9 – used in La Hague and Marcoule

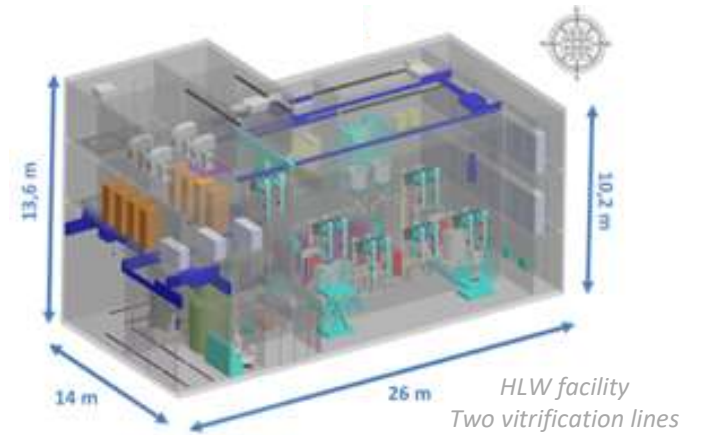
Industrial design

Design Requirements

- Simple and compact equipment
- Modular design
- ↓ Investment and operation costs
- ↑ Maximize availability
- ↓ Occupational exposure and environmental impact
- ↓ Secondary waste

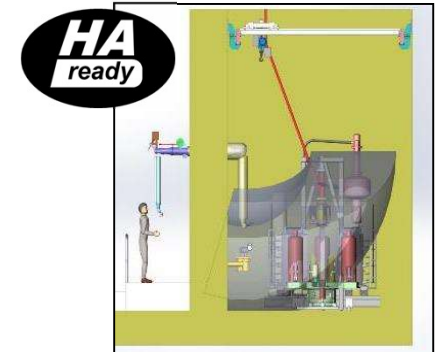


Smaller vitrification cells and very compact facilities



Fully adapted for High Active waste

- Remotely operation & maintenance
- In-cell assembly and disassembly with moderate sized:
 - Overhead cranes
 - Master-slave manipulators
 - Remotely controlled tools



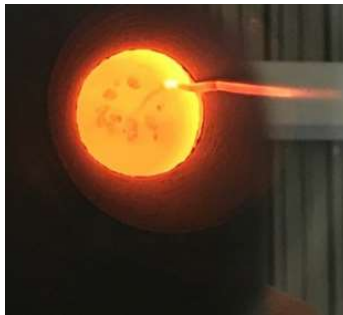
DEM&MELT main achievements

► **Several kinds of waste tested at different scale:**

- Alpha liquid waste
- Solid fission products deposits
- Liquid fission products
- Adsorbents (zeolite, silicotitanate, sand)
- Ashes from incineration process
- Sludges/Slurries from coprecipitation process

► **High Waste Loading achieved (up to 80% oxide)**

► **Very low radionuclides volatility**



← **Mix of zeolites, silicotitanates and sand**

- WLox*: 60 wt.%
- Volatility: 0.04 % for Cs and 0.01 % for Sr



↑ **ALPS ferric and carbonated slurries**

- WLox*: ~ 40 wt.%
- Sr volatility: 7.10-3 wt%

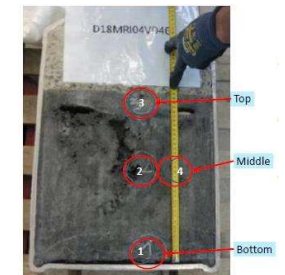
→ **Mix of zeolites, slurries, silicotitanates and sand**

- WLox*: 80 wt.%
- Volatility: <0.5 wt% for Cs and <0.1 wt% for Sr



↑ **Natural chabazite-type zeolites**

- WLox*: ~ 50 wt.%
- Cs volatility: 0.08 wt%



* $W_{Lox}(\%) = \frac{\text{sum of oxide masses composing the waste (kg)}}{\text{mass of waste form (kg)}} \times 100$

Vitrification of Fukushima Daiichi ALPS slurries

FULL SCALE PILOT TEST

Waste: ALPS ferric and carbonated slurries

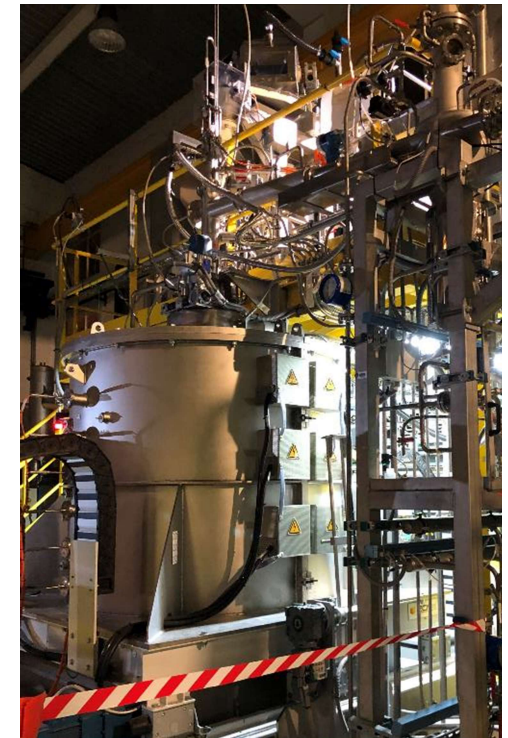
- ▶ Highly **viscous** and **sticky** → Very challenging regarding the feeding system
- ▶ High tendency to **foam** because of the high **gas release**
- ▶ High content of Sr
- ▶ Test 1 → Programmed stop and go of the feeding system
- ▶ Test 2 → Nominal operation with higher feeding rate



Waste surrogate made by coprecipitation and filtration, same as the real ALPS slurry



Waste surrogate in the feeding hopper



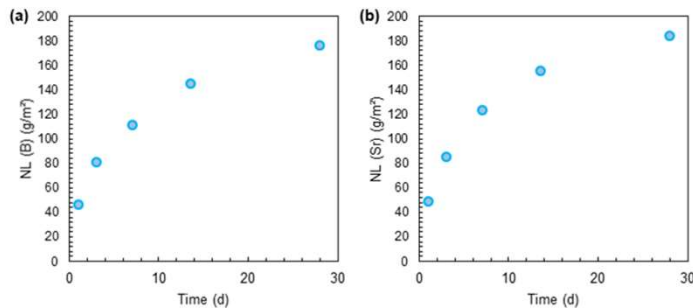
Full scale pilot

Vitrification of Fukushima Daiichi ALPS slurries

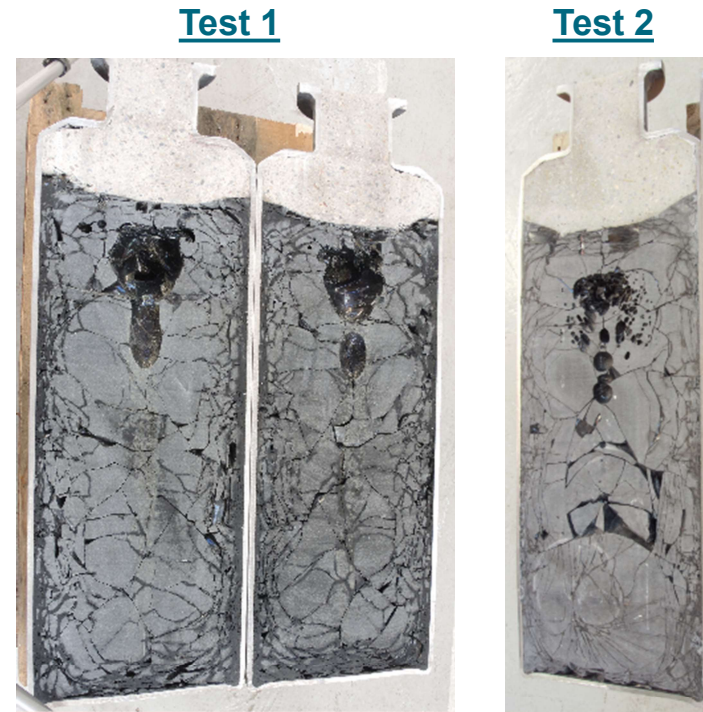
FULL SCALE PILOT TEST

Waste: ALPS ferric and carbonated slurries

- ▶ Proper operation of the feeding system even during transient modes
- ▶ No foaming issue
- ▶ **WLox***: ~ 40 wt.%
- ▶ **Sr volatility** = $7 \cdot 10^{-3}$ wt%



Leaching test results



Half-cut canister

This test has been performed by the funds from the Japanese Ministry of Economy, Trade and Industry as The Subsidy Program "Project of Decommissioning and Contaminated Water Management"

$$* WLox(\%) = \frac{\text{sum of oxide masses composing the waste (kg)}}{\text{mass of waste form (kg)}} \times 100$$

Summary

Summary

▶ **R7 and T7 outstanding records of operation & plants availability with respect to safety and glass quality**

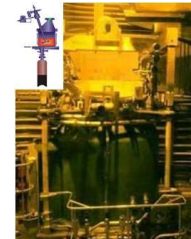
IHMM

- In operation since 1989 at LH plant
- ~ 24 100 canisters produced
- ~ 368 10⁶ TBq vitrified
- ↗ Noble Metals incorporation
- ↗ Glass throughput
- ↗ Melter (IHMM) lifetime



CCIM

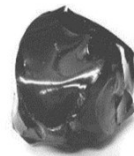
- In operation since 2010
- Retrofitted in a IHMM vitrification cell
- ~ 1 000 canisters produced
- ↗ Noble Metals incorporation & Glass throughput
- Industrial maturity
- Since 2020 → Vitrification of FP from commercial activity



▶ **Very High-Level Waste management with significant incorporation rate into the glass → Around 1 Ci/g**

▶ **DEM&MELT In-Can Vitrification Technology**

- Full-scale pilot commissioned in 2020
- Benefiting from over 40 years of HLW vitrification
- Simplicity, robustness, and versatility
- High rates of waste incorporation into the matrix



Outcome of the continuous improvement policy implemented through a close collaboration between R&D, engineering teams and the industrial operator